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Advances in Applied Science Research, 2011, 2 (2): 252-259



# Use of mixed metal oxide as a catalyst in the decomposition of hydrogen peroxide

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#### **ABSTRACT**

The decomposition of hydrogen peroxide in presence of some metal oxides as a heterogeneous & heterogenized catalyst has been investigated by measuring the evolution of oxygen at different time intervals in the temperature range  $30-60^{0}$ C. The catalytic activity is increased, an increase in the amount of catalyst and pH. The variation of  $H_2O_2$  at constant pH reveals that the values of K are nearly constant irrespective of K are suggested in which an intermediate surface complex is thought to be responsible for the enhancement of the decomposition of hydrogen peroxide. K actalyst was characterized by K and K and K and K are K are K and K are K and K are K and K are K are K and K are K are K and K are K and K are K and K are K and K are K are K and K are K are K and K are K and K are K are K and K are K and K are K and K are K are K and K are K are K and K are K and K are K are K and K are K are K and K are K and K are K and K are K are K and K are K are K and K are K are K and K are K are K are K and K are K and K are K and K are K and K are K are K and K are K and K are K and K are K and K are K are K and K are K and K are K are K and K are K are K and K

**Keywords:** Catalyst, XRD, EDX, TG/DTA, SEM, AFM, H2O2 decomposition.

### **INTRODUCTION**

Hydrogen peroxide and its solutions find use as antiseptic in medicine [1-2].hydrogen peroxide is environmentally benign oxidant, is expected to play an increasingly important role in the chemical industry, Other applications of  $H_2O_2$  such as bleach in the textile & paper/pulp industry, in treatment of waste water ([3].The sterilization of packages food, beverages, drugs etc, requires fast, reliable and inexpensive aseptic methods. The sterilization by hydrogen peroxide  $H_2O_2$ vapour offers one distinct advantage over other chemical methods [4] like gaseous formaldehyde, glutaraldehyde and ethylene oxide, namely its harmless decomposition products of  $H_2O_2$  and oxygen. On the other hand, in industrial applications  $H_2O_2$  is mixed with ambient air and heated up to more than  $200^0$ C; yielding a gaseous  $H_2O_2$  concentration varying between 1 to 10 vol. %. The controlled decomposition of  $H_2O_2$  on oxides and mixed oxides has been studied

extensively by many researchers. [5-9] .Recently the literature survey reveals that mixed oxide catalyst is more active in the reaction of  $H_2O_2$  decomposition. These catalysts have attracted much attention of the chemist due to their application as low cost fuel cells, their stability and highly activity. [10-11] .The catalytic activity of this catalyst depends on the preparative methods viz. Combustion method, Oxalate route, Co-Precipitation method, solid solution precursor wet Chemical method, Sol gel method, Microwave synthesis, Oxidation method, Spray dry etc. [12-19]. Out of these methods solution combustion method is important because catalyst is prepared within a minute, simple technique. LaCrO3 is a spinel type structure and due to their chemical stability and highly oxidative nature, it is industrially important. In this paper the kinetics of  $H_2O_2$  decomposition on LaMnO3 mixed oxide at room temperature has been investigated. In present study reports the heterogeneous and heterogenized homogenous catalysis using nanocrystalline LaCrO3 prepared from combustion method.

#### MATERIALS AND METHODS

#### **Experimental-**

Polycrystalline LaCrO $_3$  was synthesized by the combustion synthesis method using glycine as fuel (organic fuel). All chemical reagents were analytical grade and used without further purification. Stoichiometric quantity of solid mixture of one mole reagents i.e. Lanthanum nitrate La (NO $_3$ ) $_3$ .6H $_2$ O, Cr (NO $_3$ ) $_3$ .9H $_2$ O and two mole of glycine were mixed together in a flat Pyrex disc. The solid were stirred for five minutes (clear solution was obtained). Solution formed was evaporated on hot plate in temperature range 80-90 C gives thick gel. The gel was kept on a hot plate for auto combustion and heated in the temperature range of 160-180 C. The nanocrystalline LaCrO $_3$  powder was formed within five minutes.

#### Kinetic Measurement-

A weight quantity of the catalyst was shaken with  $10 \text{ cm}^3 \text{ H2O2}$  (5 Vol) in a closed vessel kept in a thermostatic water bath and the volume of oxygen evolved was measured by using gasometric technique [20]. Experiment were carried out at three different temperatures (T) in the range 30-60 $^{\circ}$ C. The effect of changing in the amount of catalyst was studied at constant concentration of  $H_2O_2$ at  $55^{\circ}$ C. The specific reaction rates (k) were calculated from the plot of log (a-x) verses time t ,where a and x are the volumes of oxygen evolved after completion of decomposition and at any time t,respectively. The ln k values were plotted against 1/T (Arrhenius plot). The slope of Straight line obtained is -E/R. Thus, the activation energy (E) was calculated from slope. The activation parameters,  $\Delta H\#$ ,  $\Delta S\#$ , were calculated by Eyring equation(21).

#### **RESULT AND DISCUSSION**

When reactants were heated at 180°C the reaction proceeds by the mechanism indicated by equation number 1 and 2 give the final product LaCrO3.

$$2C_2NH_5O_2 + (9/2) O_2 \rightarrow N_2\uparrow + 4CO_2\uparrow + 5H_2O\uparrow$$
 (1)

La 
$$(NO_3)_3 + Cr (NO_3)_3 + 4 C_2H_5NO_2 \rightarrow LaCrO_3 + 8CO_2\uparrow + 10H_2O\uparrow +5 N_2\uparrow$$
 (2)

The TG curve recorded for thermal decomposition of LaCrO<sub>3</sub> is shown in Fig.1. The curve indicates that the slight weight loss in LaCrO<sub>3</sub> powder due to little loss of moisture, carbon dioxide and nitrogen gas. The DTA curve of LaCrO<sub>3</sub> recorded in static air, curve shows that LaCrO<sub>3</sub> did not decompose, but weight loss was due to dehydrogenation decarboxylation and denitration and yield final product at 775°C. This weight loss and weight gained was very negligible. This weight change was in the range of 0.02 % only. These indicate that the synthesized powder was almost stable from the beginning.

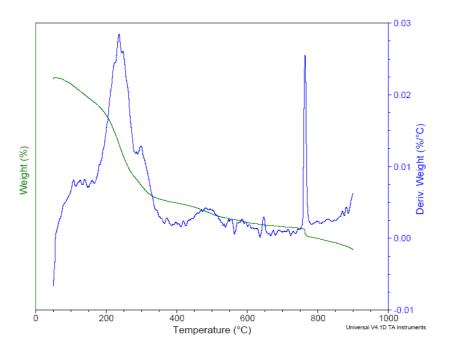


Fig. 1 TG - TDA curve of LaCrO<sub>3</sub> as synthesized powder.

X-ray diffraction XRD measurements were performed on Philips Analytic X-ray B.V. (PW-3710 Based Model) Advanced X-ray diffraction using Cu K $\alpha$  1.54056, radiation. The XRD pattern shown in the fig.(2).The XRD pattern shows that the product is pure spinel oxide LaCrO $_3$  with an orthorhombic structure. The diffraction data are good agreement with JCPD card of LaFeO $_3$  (JCPDS No.24-1016) The average crystalline size of LaCrO $_3$  spinel powder was estimated with the help of Scherrer's equation t =0.9 $\lambda$ / $\beta$   $cos\theta$  [22-23] where t is the thickness of the crystals (in angstroms),  $\lambda$  is the X-ray wavelength and  $\theta$  is the Bragg angle  $\beta$  is the integral breath that depends on the width of the most predominant peak at 100% intensity =1.54056 A $^\circ$ . The average particle size 0f nanocrystalline LaCrO $_3$  was ~16 nm. LaCrO $_3$  nanocrystals are more attractive in the field of catalytic application. Fig.3 shows Energy Dispersive X-ray (EDX) technique that allows the determination of chemical composition of LaCrO $_3$  Catalyst.

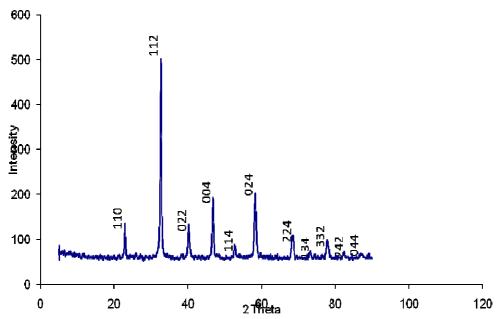


Fig. 2 X-ray diffraction patterns of LaCrO<sub>3</sub> as synthesized powder.

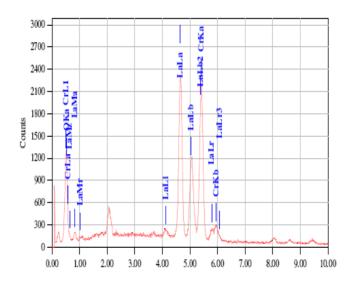


Fig.-3 Energy Dispersive X-ray (EDX) of LaCrO<sub>3</sub> Catalyst

The surface morphology was studied by using scanning electron microscopy (SEM) Model No. JEOL, JSM.6360. The SEM images of LaCrO<sub>3</sub> are shown in fig. (4). The SEM images reveal the product is a low density, loose and porous material that is favorable to a catalyst application. The BET surface areas were measured on a Benchman coulter SA 3100 plus instrument using nitrogen adsorption at  $200^{\circ}$  C. the surface area of the synthesized powder was 3.5 m<sup>2</sup>/g.

Scanning Electron Microscope (SEM) image of the  $LaCrO_3$  powder prepared by combustion method at  $180^{\circ}C$  is presented in Fig.4. (a) and SEM images at  $510^{\circ}C$  and  $1000^{\circ}C$  are shown in

fig.4(b) and fig. 4(c) respectively. It shows that average particle size of LaCrO<sub>3</sub> formed is  $\sim$ 16nm. The particle size was also calculated from atomic force microscopy (AFM) recorded at 450 °C and 1000 °C temperatures. AFM images are shown in fig.5. Particle size increases as the temperature increases.

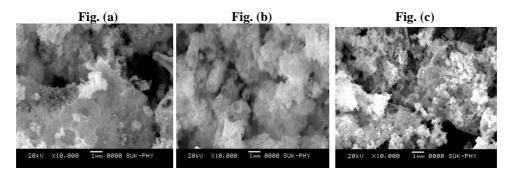


Fig.4 SEM images of LaCrO<sub>3</sub> Fig.4 (a) as synthesized powder, Fig.4 (b) at 510<sup>o</sup>C, Fig.2 (c) at 1000<sup>o</sup>C

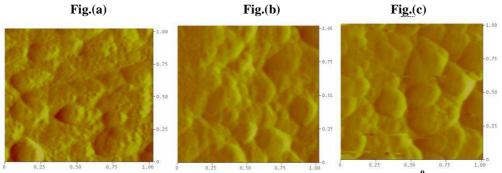


Fig.- 5: AFM images of LaCrO3 Fig.(a) as synthesized powder, Fig.(b) heated at 450 C and Fig.(c) heated at

#### LaCrO3 oxide as heterogeneous catalysts in decomposition of H<sub>2</sub>O<sub>2</sub>

In presence of LaCrO3 in heterogeneous phase, the catalytic disproportionation is increased considerably. The results of the present study on kinetic of catalytic decomposition of  $H_2O_2$  in presence of LaCrO3 as a catalyst are also given in the table. The plot of log of (a-x) versus t for LaCrO3 catalyst is linear indicating that the decomposition of  $H_2O_2$  in present of catalyst follows first order kinetics. Keeping the quantity of catalyst and  $H_2O_2$  constant and varying temperature in the range  $30\text{-}60^{\circ}\text{C}$ , the value of k increases with increase in temperature Table-1. It has been also observed that the rate of decomposition decreases with increase in  $H_2O_2$ . It may be decrease in pH of the solution. It is noted that an increase in  $H_2O_2$  from 3 to 5 vol changes the pH of the solution from 6.6 to 5.4. This is also the evident from the fact that an increase in the pH of the solution from 5.4 to 9.2 increases the k value by about 7 fold the variation of  $H_2O_2$  at constant pH 8.06(controlled by phosphate buffer) Shows that the value of k are nearly constant irrespective of  $H_2O_2$ . Keeping  $H_2O_2$  and temperature constant, when the quantity of catalyst is varied in the range 0.01-0.05g, the value of k increases with increase in the quantity of catalyst Table-2. and Fig.7. The plot of log of k versus log of (amount of LaCrO3) is linear with a slope of 1.1, indicating that the order of dispropornation reaction is almost unity. Fig-(6) The values of

 $\Delta S^{\#}$  are found to be negative in all the cases indicating that molecule in transition state are more ordered than the reactant in ground state[24] Mechanism proposed for decomposition of  $H_2O_2$  catalyzed by  $LaCrO_3$  is shown in scheme 1.

H<sub>2</sub>O<sub>2</sub> auto ionizes as

$$\begin{split} &H_2O_2 \leftrightarrow H^+ + OOH^- \\ &LaCrO_3 + OOH^- + OOH^- + LaCrO_3 + H_2O_2 \rightarrow LaCrO_3 + H_2O_2 \rightarrow Deprotonation \rightarrow LaCrO_3 + H_2O_2 + OH^- + H^+ \rightarrow LaCrO_3 + H_2O_2 + OH^- \\ &The \ reaction \ is : \\ &2H_2O_2(aq) \rightarrow 2H_2O(l) + O_2(g) \end{split}$$

Table 1 Decomposition of hydrogen peroxide<sup>a</sup> catalyzed by LaCrO3 as heterogeneous catalyst<sup>b</sup>

Metal oxide	$T(^{0}C)$	K in (min <sup>-1</sup> )	E kJ/mol	$\Delta H^{\#}(kJ/mol)$	$\Delta S^{\#}(J.K^{-1}mol^{-1})$
LaCrO <sub>3</sub>	35	$6.4 \times 10^{-3}$	66.466	62.977	-93.57
	45	1.3X10 <sup>-2</sup>			
	55	$7.89X^{10-2}$			

<sup>a</sup>Volume of hydrogen peroxide: 10.0 cm3 (- 5 vol), <sup>b</sup>wt.%,0.036

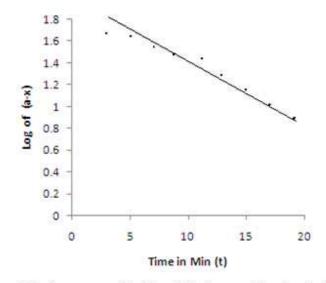
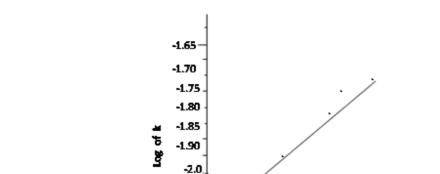


Fig. 6 plot of log of (a-x) versus time in min (t)

Table 2- Influence of the amount of heterogeneous catalyst on the decomposition  $^a$  of hydrogen peroxide by  $LaCrO_3$ 

Catalyst	Wt.%	Specific reaction rate k (min <sup>-1</sup> )	Order of reaction with respect to catalyst
	0.09	0.0095	
	0.18	0.0117	
LaCrO <sub>3</sub>	0.27	0.0146	1.1
	0.36	0.0182	
	0.45	0.0213	

<sup>&</sup>lt;sup>a</sup> Temperature: 55<sup>o</sup>C Volume of hydrogen peroxide: 10.0 cm3 (- 5 vol)



-2.05 -2.1 -1.1

Fig.7 Log k versus log of amount of LaCrO₃ catalyst

-05

-0.3

-0.7

Log of amount of LaCrQ3

-0.9

# 4.1 Reuse of catalyst

LaCrO<sub>3</sub> was separated from the reaction mixture by using microcentrifuge machine at 16000 rpm (Model, Rm-12C DX). The separated LaCrO<sub>3</sub> was dried at 110<sup>o</sup>C for one hour. It was used for many times for the same purpose and it was found that similar activity of LaCrO3 for decomposition of hydrogen peroxide. This is the green approach in chemistry.

### **CONCLUSION**

The LaCrO3 is prepared successfully by the combustion method. This method is simple, rapid. The reaction obeys the first order rate laws. The reaction generally proceeds through the formation of activated complex. LaCrO3 has an enhanced effect on the catalytic decomposition of H2O2 especially at higher temperature. The role of LaCrO3 as catalysts in the decomposition of H2O2 has been confirmed by the fact that they remain unchanged in amount and chemical composition at the end of reaction.

# **Acknowledgments**

Sanjay M. Khetre is very much thankful to UGC for sanctioning FIP under XI<sup>th</sup> Plan. He is also thankful to Dr.Patanrao Kadam Mahavidyalaya Sangli for providing research facility.

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